

Quick
Revision
Formulae
For
Mechanical Engg.

* Francis turbine

- Area of flow $\Lambda_{f1} = K\pi d_1 b_1$
- Discharge through the runner $Q = \Lambda_{f1} V_{f1}$
- Hydraulic power $[H.P = \gamma Q H]_{\text{KW}}$
- Runner power when v_{w_2} is in direction of u_1

$$R.P = \frac{\gamma Q}{g} [v_{w_1} u_1 - v_{w_2} u_2]$$

- Runner power when v_{w_2} is in opposite direction of u_2

$$R.P = \frac{\gamma Q}{g} [v_{w_1} u_1 + v_{w_2} u_2]$$

- Hydraulic efficiency $\eta_h = \frac{R.P}{H.P} = \frac{v_{w_1} u_1}{gH}$ to R.W.L

- Mechanical efficiency $\eta_{mech} = \frac{S.P}{R.P}$ M.S.E

- Overall efficiency $\eta_o = \eta_h \times \eta_{mech}$ O.S.E

- Volumetric efficiency $\eta_{vol} = \frac{Q}{Q + \Delta Q}$
 where ΔQ = leakage loss
 Q = discharge entering the turbine

- Degree of reaction (R) :
$$R = 1 + \frac{v_2^2 - v_1^2}{2v_{w_1} u_1}$$

- Efficiency of draft tube
$$\eta_d = \frac{\left(\frac{v_2^2}{2g} - \frac{v_3^2}{2g} \right) - h_f}{\frac{v_2^2}{2g}}$$

* Pelton wheel

- Power available at inlet of vanes = $\frac{\gamma Q v_1^2}{2g}$

- Runner power $R.P = \frac{\gamma Q}{g} [v_{w_1} - v_{w_2}] u$

- $(\eta_b)_{max} = \frac{1 + K \cos \theta}{2}$

- Blade efficiency $\eta_{blade} = \frac{v_1^2 - v_2^2}{v_1^2}$

Specific speed of Turbine $N_s = \frac{N\sqrt{P}}{H^{5/4}}$

Fluid Mechanics

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* Model relationships for turbine / Cp

Capacity or flow coeff. head coeff.

$$\left(\frac{Q}{ND^3} \right)_p = \left(\frac{Q}{ND^3} \right)_m \quad \left(\frac{gH}{N^2 D^2} \right)_p = \left(\frac{gH}{N^2 D^2} \right)_m$$

power coeff.

$$\left(\frac{P}{N^3 D^5} \right)_p = \left(\frac{P}{N^3 D^5} \right)_m$$

* Brayton cycle or Joule cycle:- [Gas P.P]

$$\eta = 1 - \frac{1}{(r_p)^{\frac{\gamma-1}{\gamma}}} \quad T_2 = T_4 = \sqrt{T_{\max} \cdot T_{\min}}$$

$$(r_p)_{\text{optimum}} = \left(\frac{T_{\max}}{T_{\min}} \right)^{\frac{\gamma}{2(\gamma-1)}}$$

$$(r_p)_{\text{optimum}} = \sqrt{(r_p)_{\max}} \quad (r_p)_{\max} = \left(\frac{T_{\max}}{T_{\min}} \right)^{\frac{\gamma}{\gamma-1}}$$

$$\text{Back work Ratio} = \frac{W_C}{W_T}$$

$$\text{Work Ratio} = \frac{W_{\text{net}}}{W_T} = \frac{W_T - W_C}{W_T} \quad 1 - \frac{W_C}{W_T}$$

* Rankine vapour power cycle (or) steam power cycle

Specific steam consumption $SSC = \frac{3600}{W_{\text{net}}} \frac{\text{kg}}{\text{kw.hr}}$

$$\eta_{\text{Rankine}} = 1 - \frac{Q_{\text{rej}}}{Q_{\text{in}}} = 1 - \frac{T_1}{T_m} = \frac{W_{\text{net}}}{Q_s} = \frac{Q_s - Q_R}{Q_s} = 1 - \frac{Q_R}{Q_s} \quad \text{KJ/KJ}$$

• For regeneration in Rankine cycle

$$W_T = 1(h_1 - h_2) + (1-y)(h_1 - h_7)$$

$$W_P = (1-y)(h_2 - h_1) + 1(h_4 - h_3)$$

$$W_{\text{net}} = W_T - W_P$$

$$Q_s = 1(h_2 - h_4)$$

• Applying conservation of energy for OFWH

$$(1-y)h_2 + yh_4 = 1 \cdot h_1$$

Heat & Mass Transfer

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- Average skin friction coefficient

$$(\bar{C}_{fx}) : \bar{C}_{fx} = 2C_{fx}$$

- Average heat transfer coefficient

$$(\bar{h}_x) : \bar{h}_x = 2h_x$$

- Peclet No. $Pe_x = Re_x \cdot Pr$

For turbulent boundary layer

- $C_{fx} = 0.0592 Re_x^{-1/5}$ (for $5 \times 10^5 < Re_x < 10^7$)

- $\bar{C}_{fL} = 0.074 Re_L^{-1/5}$

- $\bar{N}_{uL} = 0.037 Re_L^{4/5} Pr^{1/3}$ ($0.6 < Pr < 60$)

* Convection in pipes

(i) constant heat flux at wall

$$\frac{\bar{h}D}{K} = \bar{N}_{uD} = 4.364$$

(ii) constant wall temperature $\bar{N}_{uD} = 3.66$

For turbulent flow

$$\bar{N}_{uD} = 0.023 Re_D^{4/5} Pr^{1/3} \rightarrow \text{Dittus Boelter relation}$$

* Natural convection

- Grashof's number $Gr_L = \frac{g\beta L^3 (T_s - T_\infty)}{\nu^2}$

- Rayleigh number $Ra_L = Gr_L \cdot Pr = \frac{g\beta L^3 (T_s - T_\infty)}{\nu^2}$

* Heat exchanger

- Logarithmic mean temperature difference (LMTD)

$$Q = \dot{m}_h C_h \Delta T_h$$

$$Q = \dot{m}_c C_c (T_{c,o} - T_{c,i})$$

$$Q = \frac{UA (\Delta T_1 - \Delta T_2)}{\ln \left(\frac{\Delta T_1}{\Delta T_2} \right)}$$

* Effectiveness

- NTU method : $NTU(N) = \frac{UA}{C_{min}}$

Heat & Mass Transfer

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- For double pipe or parallel flow $\epsilon = \frac{1 - \exp[-N(1+C)]}{1+C}$

- Counter flow effectiveness $\epsilon = \frac{1 - \exp[-N(1-C)]}{1 - C \exp[-N(1-C)]}$

- $\epsilon = \frac{N}{1+N}$ (if $C=1$)

- * **Radiation**

- Lambert's cosine law $E_b = \pi I_b = \sigma T^4$

- Plank's distribution law

$$E_{b\lambda} = \pi I_{b\lambda} = \frac{2\pi C_1}{\lambda^5 \left[\exp\left(\frac{C_2}{\lambda T}\right) - 1 \right]}$$

$$C_1 = 6.625 \times 10^{-34} \text{ J.S}$$

$$C_2 = 1.88049 \times 10^4 \text{ J/mol.K}$$

- Wein's formula $\frac{I_{b\lambda}}{T^5} = \frac{2C_1}{(\lambda T)^5 \exp\left(\frac{C_2}{\lambda T}\right)}$

- Rayleigh-Jean's formula $\frac{I_{b\lambda}}{T^5} = \frac{2C_1}{C_2} \frac{1}{(\lambda T)^4}$

- Wein's displacement law

$$\lambda_{\max} T = C_3 \quad C_3 = 0.289 \times 10^{-2} \text{ m.k}$$

- Reciprocity theorem $A_1 F_{12} = A_2 F_{21}$

- Radiation exchange between small grey bodies

$$Q_{12} = \epsilon_1 \epsilon_2 A F \sigma (T_1^4 - T_2^4)$$

- Radiation exchange between large parallel gray bodies

$$Q_{12} = \frac{A \sigma (T_1^4 - T_2^4)}{\frac{1}{\epsilon_1} + \frac{1}{\epsilon_2} - 1}$$

- Radiation exchange between large gray concentric cylinders or sphere

$$Q_{12} = \frac{A_1 \sigma (T_1^4 - T_2^4)}{\frac{1}{\epsilon_1} + \frac{A_1}{A_2} \left(\frac{1}{\epsilon_2} - 1 \right)}$$

- Exchange between a small gray body in a large gray enclosures

$$Q_{12} = \epsilon_1 A_1 \sigma (T_1^4 - T_2^4)$$

- Radiosity $J = G\rho + \epsilon E_b$

- Critical radius of insulation

For cylinder $r_c = \frac{K_{ins}}{h}$ For sphere $r_c = \frac{2K_{ins}}{h}$

Heat & Mass Transfer

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- Fourier's law $Q = -KA \frac{dT}{dx}$

- Newton's law of cooling $\frac{Q}{A} = q = h(T_s - T_\infty) = h \Delta t$

- Stefan-Boltzmann law

$$Q = \sigma A T_1^4 \quad \sigma = 5.67 \times 10^{-8} \text{ W/m}^2 \text{K}^4$$

- $Q = UA \Delta T$ U = over all heat transfer coefficient

$$U = \frac{1}{\frac{1}{h_A} + \frac{1}{k} + \frac{1}{h_B}}$$

- General 3-D heat conduction equation

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{q}{k} = \frac{\rho C_p}{K} \frac{\partial T}{\partial t} = \frac{1}{\alpha} \frac{\partial T}{\partial t}$$

- α = thermal diffusivity $= \frac{K}{\rho C_p} (\text{m}^2/\text{sec})$

- Heat conduction through plane wall $Q = \frac{KA \Delta T}{L}$

- For cylinder $\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) = 0$

- For sphere $\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial T}{\partial r} \right) = 0$

- Radial heat conduction through cylindrical system

$$Q = \frac{2\pi K L (T_i - T_o)}{\ln \left(\frac{r_o}{r_i} \right)}$$

- For sphere $Q = \frac{4\pi K r_i r_o (T_i - T_o)}{r_o - r_i}$

- System with variable thermal conductivity

$$K_m = k (1 + \beta T_m)$$

- Plane wall with internal heat generation

$$\frac{d^2 T}{dx^2} + \frac{q}{k} = 0 \quad T_w = T_\infty + \frac{qL}{2h}$$

- Biot no. $Bi = \frac{hL}{K} \quad T_{max} = T_w + \frac{qL^2}{8K}$

* FINS

Long fins: $\frac{T - T_\infty}{T_0 - T_\infty} = e^{-mx}, \quad m = \sqrt{\frac{hp}{kA}}$

$$Q = \sqrt{hpkA} \theta_0 = \sqrt{hpkA} (T_0 - T_\infty)$$

- **Fin with insulated end:**

$$\frac{T - T_\infty}{T_0 - T_\infty} = \frac{\cosh[m(L - x)]}{\cosh(mL)}$$

$$Q = \sqrt{hpkA} (T_0 - T_\infty) \tanh(mL)$$

- **Fin with convection off the end:**

$$Q = \sqrt{hpkA} (T_0 - T_\infty) \frac{\tanh(mL) + \frac{h}{mk}}{1 + \left[\tanh(mL) \right] \frac{h}{mk}}$$

- **Efficiency of fins** $(\eta_{fin}) = \frac{Q_{fin}}{Q_{max}}$

$$Q_{max} = hPL\theta_0$$

- **Effectiveness of fins (E)** $E = \frac{Q_{with fin}}{Q_{without fin}}$

- **Skin friction coefficient (C_f)** $C_f = \frac{\tau_s}{\frac{1}{2}\rho u_\infty^2}$

- **Prandtl No. (P_r)** $P_r = \frac{v}{\alpha} = \frac{\mu C_p}{K}$

- **Friction factor for laminar flow** $f = \frac{64}{Re}$

- **Darcy-weisbach equation**

$$h_{fL} = \frac{f L u_\infty^2}{2gD}$$

- **Bulk mean temperature** $T_b = \frac{2}{u_\infty R^2} \int_0^R u T r dr$

- **Mean velocity (u_m)** $u_m = \frac{2}{R^2} \int_0^R u r dr$

- * **Forced convection system**
Exact laminar boundary layer solution

- **Boundary layer thickness**

$$(\delta) \quad \delta = \frac{5.0}{\sqrt{u_\infty / \nu x}} = \frac{5x}{\sqrt{Re_x}}$$

- **Skin friction coefficient** $C_{fx} = \frac{\tau_s}{\frac{1}{2}\rho u_\infty^2} = \frac{0.664}{\sqrt{Re_x}}$

* **Otto cycle :**

$$R_k = \frac{V_C + V_S}{V_C} = \frac{V_1}{V_2}$$

$R_k = \text{C.R (Compression Ratio)}$

$$\eta = 1 - \frac{1}{(R_K)^{\gamma-1}}$$

• **Mean effective pressure**

$$P_{\text{mean}} = \frac{\eta(\Delta P)}{(\gamma-1)(R_k-1)}$$

* **Diesel cycle:**

$$R_c = \text{cut off ratio} = \frac{V_3}{V_2}$$

$$\eta = 1 - \frac{1}{(R_k)^{\gamma-1}} \gamma \left[\frac{R_c^\gamma - 1}{R_c - 1} \right]$$

* **Performance parameters**

1. Indicated power $IP = \frac{P_{imep} \times L \times A \times K \times n}{60}$

2. Brake power

$$B.P = \frac{P_{b,mep} \times L \times A \times k \times n}{60} \quad \text{or} \quad BP = \frac{2\pi NT}{60}$$

3. Friction power $F.P = IP - BP$

4. Mechanical efficiency $\eta_m = \frac{BP}{IP}$

5. Indicated thermal efficiency (η_{ith})

$$\eta_{ith} = \frac{IP}{\dot{m}_f \times CV}$$

Internal Combustion Engine

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6. Brake thermal efficiency

$$\eta_{bth} = \frac{BP}{\dot{m}_f \times CV}$$

7. Relative efficiency ($\eta_{rel.}$) = $\frac{\text{Actual thermal } \eta}{\eta_{air \text{ standard}}}$

8. Volumetric efficiency

$$\eta_{vol} = \frac{\text{Volume of charge actually inducted}}{V_s}$$

9. Indicated specific fuel consumption

$$(ISFC) = \frac{\dot{m}_f}{SP}$$

10. Brake specific fuel consumption

$$BSFC = \frac{\dot{m}_f}{BP}$$

11. Specific power output:

$$P_s = \frac{B.P}{A}$$

*** Comparison of factors controlling the knocking for S.I & C.I engines**

Factors	S.I Engine	C.I Engine
(1) SIT	High	Low
(2) Delay period	High	Low
(3) R_k	Low	High
(4) inlet temperature & pressure	Low	High
(5) combustion wall temperature	Low	High
(6) rpm (N)	High	Low
(7) cylinder size	Small	Large

- **Length of open belt drive (O.B.D)**

$$= 2C + \frac{\pi}{2}(D_1 + D_2) + \frac{(D_2 - D_1)^2}{4C}$$

- **Length of cross belt driven (C.B.D)**

$$= 2C + \frac{\pi}{2}(D_1 + D_2) + \frac{(D_2 + D_1)^2}{4C}$$

- **Velocity ratio**

$$V.R = \frac{N_2}{N_1} = \left(\frac{D_1 + t}{D_2 + t} \right) \left(1 - \frac{S}{100} \right)$$

- **Ratio of belt tension** $\frac{T_1}{T_2} = e^{\mu\theta}$

- **Maximum tensile strength of belt**

$$T_{\max} = b \cdot t \cdot \sigma_{\text{per}}$$

- **Power transmission capacity of belt drive**

$$P.T.C = (T_1 - T_2)v$$

- **Centrifugal tension** $T_c = \frac{T_{\max}}{3}$

- **Initial tension** $T_0 = \frac{T_1 + T_2 + 2T_c}{2}$

- **Number of 'V' belts** $n = \frac{P_{\text{total}}}{P_{\text{each}}} \times K_q$

- **Buckingham dynamic load**

$$F_d = F_t + \frac{20.67v[bc + F_t]}{20.67v + \sqrt{bc + F_t}}$$

$$c = \frac{e}{K \left[\frac{1}{E_1} + \frac{1}{E_2} \right]}$$

- **Soderberg equation** $\frac{1}{FOS} = \frac{\sigma_m}{\sigma_{yt}} + \frac{K_f \sigma_v}{\sigma_e}$

- **Goodman equation** $\frac{1}{FOS} = \frac{K_t \sigma_m}{\sigma_{ut}} + \frac{K_f \sigma_v}{\sigma_e}$

- **Notch sensitivity index** $q = \frac{K_f - 1}{K_t - 1}$

- **Unwin's formula** $d = 6\sqrt{t}$

- **Area of transverse fillet weld**

$$A_{T.F.W} = h\ell_e, \quad h = \frac{t}{\cos \theta + \sin \theta}$$

- $\text{Strength of T.F.W} = 0.832t\ell_e\tau_{per}$

- **Strength of parallel fillet weld**
 $= 0.707t\ell_e\tau_{per}$

- **Strength of Butt weld** $= h\ell(\sigma_t)_{per}$

- **Frictional torque of thrust bearing by uniform pressure theory**

$$(T_f)_{UPT} = \frac{2}{3}\mu\omega \left(\frac{R_o^3 - R_i^3}{R_o^2 - R_i^2} \right)$$

- **Frictional torque of thrust bearing by uniform wear theory**

$$(T_f)_{UWT} = \mu\omega \left(\frac{R_o + R_i}{2} \right)$$

- **Power loss** $P_{loss} = T_f \cdot \omega$

- * **T_f equations for flat pivot bearing**

$$(T_f)_{UPT} = \frac{2}{3}\mu WR$$

$$(T_f)_{UWT} = \frac{1}{2}\mu WR$$

- **Bearing pressure** $p_{ind} = \frac{W}{LD}$

- **Strength of bearing** $= p_{per} \times L \times D$

- **Bearing characteristic number** $= \frac{zn}{p}$

- **Mc-Kee's equation**

$$\mu = \frac{33}{10^8} \left[\left(\frac{zn'}{p'} \right) \left(\frac{D}{C} \right) \right] + K$$

- **Somer field No.** $S = \left(\frac{zn}{p} \right) \left(\frac{D}{C} \right)^2$

- **Petroff's equation for μ** $\mu = \frac{2\pi^2}{\tau_{ps}} \left(\frac{zn}{p} \right) \left(\frac{D}{C} \right)$

- **Life of bearing** $L_{50} = \left(\frac{C}{P_e} \right)^k$ (Million rev.)

Refrigeration & Air Conditioning

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• $(COP)_{ref} = \frac{R.E}{W_{in}}$ • Unit of refrigeration = TR, $1TR = 3.5 \text{ KJ / sec}$

• Volumetric efficiency of a reciprocating compressor

$$\eta_{vol} = \frac{\text{Actual volume}}{\text{Swept volume}} = \frac{\dot{m} v_1}{\frac{\pi}{4} D^2 L N K}$$

$$\eta_{vol} = 1 + C - C \left(\frac{P_2}{P_1} \right)^{1/n}, \quad C = \frac{V_c}{V_s}$$

• V-C cycle $COP = \frac{R.E}{W_{in}} = \frac{h_1 - h_3}{h_2 - h_1}$

• Refrigeration capacity = $\dot{m} (h_1 - h_2) \text{ kw}$

• Power input $(P_{in}) = \dot{m} (h_2 - h_1) \text{ kw}$

• Gas refrigeration cycle $w_{in} = w_c - w_E = (h_2 - h_1) - (h_3 - h_4)$ R.E. = $h_1 - h_4$

• $COP = \frac{1}{(r_p)^{\frac{\gamma-1}{\gamma}} - 1}$ • V-A refrigeration cycle $COP = \left(\frac{T_G - T_O}{T_G} \right) \left(\frac{T_R}{T_O - T_R} \right)$

• Heat rejection ratio or factor $HRR = \frac{Q_c}{R.E} = \frac{1}{COP} + 1$

• Specific humidity or humidity ratio $\omega = 0.622 \left(\frac{P_v}{P - P_v} \right)$

• Relative humidity $\phi = \frac{m_v}{m_{vs}} = \frac{P_v}{P_{vs}}$

• Degree of saturation $\mu = \frac{\omega}{\omega_s} = \phi \left(\frac{P - P_{vs}}{P - P_v} \right)$

• Enthalpy of moist air $h_m = \left[C_{Pa} t + \omega (2500 + 1.88t) \right] \frac{\text{KJ}}{\text{kg} - k}$

• Apjohn's formula $P_v = P_v' - \frac{1.8P(t - t')}{2700}$ $t' = \text{WBT}$
 $t = \text{DBT}$

• Sensible heat factors $SHF = \frac{SH}{SH + LH}$

• Room sensible heat factor $RSHF = \frac{RSH}{RTH}$

• $RLH = RTH - RSH$

• $SH = 0.024 \times \text{cmm} (\Delta t) \text{ kw}$ cmm = volume flow rate of air in m^3 / min

• $LH = 50 \times \text{cmm} (\Delta \omega)$

• Number of air changes = $\frac{\text{volume flow rate of air} (\text{m}^3 / \text{hr})}{\text{volume of room} (\text{m}^3)}$

• Bypass factor $BPF = \frac{t_s - t_2}{t_s - t_1}$ • $\eta = 1 - BPF$, $\eta = \frac{t_2 - t_1}{t_s - t_1}$

- **Normal stress when**
 σ_x, σ_y & τ_{xy} are given

$$\sigma_n = \frac{1}{2}(\sigma_x + \sigma_y) + \left(\frac{\sigma_x - \sigma_y}{2} \right) \cos 2\theta + \tau_{xy} \sin 2\theta$$

- $\tau_\theta = - \left(\frac{\sigma_x - \sigma_y}{2} \right) \sin 2\theta + \tau_{xy} \cos 2\theta$

- **Location of principal plane**

$$\tan 2\theta = \frac{2\tau_{xy}}{\sigma_x - \sigma_y}$$

- $\sigma_{1/2} = \left(\frac{\sigma_x + \sigma_y}{2} \right) \pm \sqrt{\left(\frac{\sigma_x - \sigma_y}{2} \right)^2 + \tau_{xy}^2}$

- **Absolute**

$$\tau_{\max} = \text{larger of } \left[\left| \frac{\sigma_1 - \sigma_2}{2} \right|, \left| \frac{\sigma_2 - \sigma_3}{2} \right|, \left| \frac{\sigma_3 - \sigma_1}{2} \right| \right]$$

- **Shear strain** $\gamma_{xy} = 2\tau_{xy}$

- **Maximum shear stress**

$$\tau_{\max} = \frac{\sigma_1 - \sigma_2}{2}$$

- **Centre of Mohr's circle** = $\left(\frac{\sigma_x + \sigma_y}{2}, 0 \right)$

- **Radius of Mohr's circle**

$$= \sqrt{\left(\frac{\sigma_x - \sigma_y}{2} \right)^2 + \tau_{xy}^2}$$

- **Relationship between $\sigma_{1,2,3}$ & $\epsilon_{1,2,3}$**

$$\epsilon_1 = \frac{\sigma_1}{E} - \mu \frac{\sigma_2}{E} - \mu \frac{\sigma_3}{E}, \quad \epsilon_2 = \frac{\sigma_2}{E} - \mu \frac{\sigma_3}{E} - \mu \frac{\sigma_1}{E},$$

$$\epsilon_3 = \frac{\sigma_3}{E} - \mu \frac{\sigma_1}{E} - \mu \frac{\sigma_2}{E}$$

- **Volumetric strain of rectangular bar**

$$\epsilon_v = \left(\frac{\sigma_x + \sigma_y + \sigma_z}{E} \right) (1 - 2\mu)$$

- **Volumetric strain of cylindrical bar**

$$\epsilon_v = \epsilon_l + 2\epsilon_D$$

- **Volumetric strain of spherical bar**

$$\epsilon_v = 3\epsilon_D$$

Strength Of Materials

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- * Relationship between elastic constant

$$E = 3K(1 - 2\mu), \quad E = 2G(1 + \mu), \quad E = \frac{9KG}{3K + G}$$

$$\mu = \frac{1}{m} = \frac{3K - 2G}{6K + 2G}$$

- Axial elongation of the Prismatic bar

$$\Delta = \frac{PL}{AE}$$

- * Deflection In Non-prismatic Bars

1. Stepped Bar $\Delta = \frac{PL_1}{A_1E} + \frac{PL_2}{A_2E}$

2. Circular tapering Bar $\Delta = \frac{4PL}{\pi E(D_1D_2)}$

- * Deflection of composite Bar

$$\Delta_1 = \Delta_2 = \Delta = \frac{PL}{A_1E + A_2E}$$

- * Deflection due to self weight of bar

(1) prismatic Bar $\Delta = \frac{WL}{2AE}$

(2) conical Bar $\Delta = \frac{WL}{6AE}$

- Maximum strain energy in elastic

region = $\frac{(\sigma_{EL})^2}{2E} \times \text{volume}$ or $= \frac{1}{2} P_{EL} \cdot \delta_{EL}$

- Thermal expansion $\delta_{\text{thermal}} = \alpha \Delta T L$

- Thermal strain $\epsilon_{\text{thermal}} = \pm \alpha \Delta T$

- Thermal stress $\sigma_{\text{thermal}} = \pm \alpha \Delta T E$

- In case of pure bending

$$(\sigma_b)_{\max} = \frac{M}{Z} = \frac{32M}{\pi D^3}, \quad Z = \frac{\pi}{32} D^3$$

- In case of pure torsion

$$\tau_{\max} = \frac{T}{Z_p} = \frac{16T}{\pi D^3}, \quad Z_p = \frac{\pi}{16} D^3$$

- Bending equation

$$\frac{\sigma_b}{y} = \frac{M}{I} = \frac{E}{R}$$

Strength Of Materials

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$$\frac{\sigma_{\text{Top}}}{\sigma_{\text{Bottom}}} = \frac{\epsilon_{\text{Top}}}{\epsilon_{\text{Bottom}}} = -\frac{y_{\text{Top}}}{y_{\text{Bottom}}}$$

- **Pure torsion equation for circular shaft** $\frac{T_R}{J} = \frac{\tau}{R} = \frac{G\theta}{L}$

* Combined Bending & Torsion

$$\sigma_1 / \sigma_2 = \frac{16}{\pi D^3} \left[M \pm \sqrt{M^2 + T^2} \right]$$

$$\tau_{\text{max}} = \frac{\sigma_1 - \sigma_2}{2} = \frac{16}{\pi D^3} \left[\sqrt{M^2 + T^2} \right]$$

- **Equivalent moment**

$$M_o = \frac{1}{2} \left[M + \sqrt{M^2 + T^2} \right]$$

- **Equivalent torque** $T_o = \sqrt{M^2 + T^2}$

- **Strain energy stored due to torsion in shaft**

$$u = \frac{T^2 L}{2GI_P}$$

- **Strain energy stored due to torsion in hollow shaft**

$$u_{\text{hollow}} = \frac{\tau_{\text{max}}}{4G} \left(\frac{R_o^2 + R_i^2}{R_o^2} \right)$$

- $u = \frac{\tau_{\text{max}}^2}{4G}, \tau = \frac{r}{R} \cdot \tau_{\text{max}}$

* Shear stress distribution in Beams

(1) In rectangular section

$$q = \frac{6S}{bd^3} \left(\frac{d^2}{4} - y^2 \right)$$

where S = shear force

$$q_{\text{max}} = \frac{3}{2} \frac{S}{bd}, q_{\text{avg}} = \frac{S}{bd}$$

(2) In circular Beam

(2) In circular Beam

$$q = \frac{4}{3} \frac{S}{\pi R^4} (R^2 - y^2) \quad q_{\max} = \frac{4}{3} \frac{S}{\pi R^2}$$

(3) In triangular section

$$q_{\max} = \frac{3S}{bh}, \quad q_{\text{avg}} = \frac{2S}{bh}, \quad q_{N.A} = \frac{4}{3} q_{\text{avg}}$$

(4) In Diamond section

$$q_{\max} = \frac{9}{4} \frac{S}{h^2}, \quad q_{\text{avg}} = \frac{2S}{h^2}, \quad q_{N.A} = q_{\text{avg}}$$

(5) In I-section

$$q_{\max} = \frac{S}{8I} \frac{B}{b} (b^2 - d^2) + \frac{S}{8I} d^2$$

*** Thin cylindrical pressure vessels**

$$\sigma_h = \frac{pD}{2t}, \quad \sigma_L = \frac{pD}{4t}, \quad \tau_{\max} = \frac{pD}{8t}$$

$$\epsilon_h = \frac{pD}{4tE} (2 - \mu), \quad \epsilon_L = \frac{pD}{4tE} (1 - 2\mu), \quad \epsilon_v = \frac{pD}{4tE} (5 - 4\mu)$$

*** Thin spherical pressure vessels**

$$\sigma_h = \sigma_L = \frac{pD}{4t} \quad \text{or} \quad \sigma_1 = \sigma_2 = \frac{pD}{4t}$$

• Euler's Buckling load $P_o = \frac{n^2 \pi^2 E I}{L_o^2}$

• End condition of columns

1. If both end are hinged $L_o = L$

2. If one end is fixed & other is hinged

$$L_o = L / \sqrt{2}$$

3. If both end are fixed $L_o = \frac{L}{2}$

4. If one end is fixed and other is free

$$L_o = 2L$$

• Stiffness of spring $K = \frac{P}{\Delta} = \frac{Gd^4}{64R^3n}$

Thermodynamics

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- Temperature Kelvin = °C + 273.15
- Non flow work or closed system work in various processes

1. Constant pressure or Isobaric process $w = \int p dv$

2. Constant volume Process $w = \int p dv = 0$

3. Isothermal process $w = pv \ln \left(\frac{P_1}{P_2} \right)$

4. Adiabatic process $w = \frac{P_1 V_1 - P_2 V_2}{\gamma - 1}$

5. Polytrophic process $w = \frac{P_1 V_1 - P_2 V_2}{n - 1}$

- Slope of isothermal line on P-V diagram = $-\frac{P}{V}$
- Slope of adiabatic curves on P-V diagram = $\gamma \left(-\frac{P}{V} \right)$
- For adiabatic process of an Ideal gas

1. $P_1 V_1^\gamma = P_2 V_2^\gamma$ 2. $T_1 V_1^{\gamma-1} = T_2 V_2^{\gamma-1}$

3. $\left(\frac{P_2}{P_1} \right)^{\frac{\gamma-1}{\gamma}} = \frac{T_2}{T_1}$

- Open system work in various process

1. Constant pressure process $w = -\int v dp = 0$

2. Const. volume process $w = (P_1 - P_2) V$

3. Isothermal process work $w = P_1 V_1 \ln \frac{V_2}{V_1}$

4. Adiabatic open system work

$$w = -\frac{\gamma}{\gamma-1} (P_1 V_1 - P_2 V_2)$$

5. Polytropic open system work

$$w = \frac{n}{n-1} (P_2 V_2 - P_1 V_1)$$

• $\gamma = \frac{C_p}{C_v}$, $C_p > C_v$, $\gamma > 1$, $C_p - C_v = R$, $C_v = \frac{R}{\gamma-1}$, $C_p = \frac{\gamma R}{\gamma-1}$

• 1st law of thermodynamics $\delta Q = dE + \delta w$

• II law of thermodynamics

1. Kelvin plank statement $\eta_{HE} = \frac{Q_1 - Q_2}{Q_1}$

2. Clausius statement

$$(COP)_{HP} = \frac{Q_1}{Q_1 - Q_2} \quad (COP)_{HP} - (COP)_{HE} = 1$$

Thermodynamics

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- Steady flow energy equation**

$$h_1 + \frac{\bar{V}_1^2}{2} + gz_1 + \frac{Q}{m} = h_2 + \frac{\bar{V}_2^2}{2} + gz_2 + \frac{w}{m}$$

- For unsteady state** 1. $\left(\frac{dm}{dt}\right)_{cv} = m_i - m_e$

$$2. \left(\frac{dv}{dt}\right)_{cv} = \dot{m}_i h_i + \dot{Q} + \dot{m}_e h_e - \dot{w}_{cv}$$

- Clausius inequality** $\oint \frac{dQ}{T} \leq 0$

- Entropy** $\frac{dQ}{T} \geq ds$ • **Enthalpy** $[H = U + PV]$ joule

- Specific enthalpy** $h = \frac{H}{m}$ $\frac{KJ}{kg}$

- Available energy (AE) = Q_1 - unavailable energy (UE)**

$$\uparrow UE = T_0 Q_1 \left(\frac{T_1 - T_2}{T_1 T_2} \right)$$

- Availability in closed system**

$$w_{max} = (U_1 - U_0) - T_0 (S_1 - S_0) \quad \text{useful work} \quad w_{max} = P_0 (\Delta v)$$

- Maximum work = change in availability**

- Availability in open system**

$$w_{max} = (h_1 - h_2) - T_0 (S_1 - S_2)$$

- Irreversibility** $I = T_0 (\Delta S)_{universe}$

- Gibbs function** $G = H - TS$

- Helmholtz function** $F = U - TS$

- Maxwell equations**

$$1. \left(\frac{\partial T}{\partial V}\right)_S = -\left(\frac{\partial P}{\partial S}\right)_V \quad 2. \left(\frac{\partial T}{\partial P}\right)_S = \left(\frac{\partial V}{\partial S}\right)_P$$

$$3. \left(\frac{\partial V}{\partial T}\right)_P = -\left(\frac{\partial S}{\partial P}\right)_T \quad 4. \left(\frac{\partial P}{\partial T}\right)_V = \left(\frac{\partial S}{\partial V}\right)_T$$

$$Tds = du + pdv, \quad Tds = dh - vdp$$

$$Tds = C_V dT + T \left(\frac{\partial P}{\partial T}\right)_V dv, \quad Tds = C_P dT - T \left(\frac{\partial V}{\partial T}\right)_P dp$$

$$C_P - C_V = -T \left(\frac{\partial V}{\partial T}\right)_P^2 \left(\frac{\partial P}{\partial V}\right)_T$$

$$\text{Coefficient of volume expansivity} \quad \beta = \frac{1}{V} \left(\frac{\partial V}{\partial T}\right)_P$$

$$\text{Isothermal Bulk modulus} \quad K_T = -V \left(\frac{\partial P}{\partial V}\right)_T$$

$$\text{Isothermal compressibility} \quad \frac{1}{K_T} = -\frac{1}{V} \left(\frac{\partial V}{\partial P}\right)_T$$

$$C_P - C_V = T\beta^2 V K_T$$

- Grubler's equation $[F = 3(l - 1) - 2j - h]$
- Grashof's law $[(S + l) < (p + q)]$
- Number of instantaneous centre $\begin{matrix} = LC_2 \\ \text{No. of I.C.} = \frac{l(l-1)}{2} \end{matrix}$
- Linear velocity of instantaneous centre $[V_{I_{mn}} = \omega_m (I_{mn} I_{lm}) = \omega_n (I_{mn} I_{ln})]$
- Coriolis acceleration $[a = 2V_c \omega]$
- Minimum number of teeth of gear to avoid interference $T_{\min} = \frac{2A_G}{\left\{ \sqrt{1 + \frac{1}{G} \left(\frac{1}{G} + 2 \right) \sin^2 \phi} - 1 \right\}}$
- Minimum number of teeth of pinion to avoid interference $t_{\min} = \frac{2A_P}{\sqrt{1 + G(G+2) \sin^2 \phi} - 1}$
- Speed ratio or velocity ratio $= \frac{\omega_{\text{main driver}}}{\omega_{\text{main driven}}}$
- Train value $= \frac{1}{\text{Velocity Ratio}}$
- For watt governor $[N^2 = \frac{895}{1-b}]$
- Porter governor $N^2 = \frac{895}{h} \left[\frac{2mg + (Mg \pm f)(1+K)}{2mg} \right]$ where $K = \frac{\tan \beta}{\tan \theta}$
- Proell governor $N^2 = \frac{895}{h} \left(\frac{a}{b} \right) \left[\frac{2mg + (Mg \pm f)(1+K)}{2mg} \right]$
- Stiffness of Hartnell governor $[S = 2 \left(\frac{F_2 - F_1}{r_2 - r_1} \right) \left(\frac{a}{b} \right)^2]$
- For Wilson Hartnell governor $\left[\frac{F_2}{r_2} - \frac{F_1}{r_1} = 4s + \frac{Sa}{2} \left(\frac{b}{a} - \frac{y}{x} \right)^2 \right]$
- Sensitivity of governor $= \frac{N_{\text{max}}}{N_1 - N}$

Theory Of Machine

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- **Velocity of piston**
$$v = r\omega \left[\sin \theta + \frac{\sin 2\theta}{2\sqrt{n^2 - \sin^2 \theta}} \right]$$
- **Acceleration of piston**
$$a = r\omega^2 \left[\cos \theta + \frac{\cos 2\theta}{n} \right]$$
- **Velocity of connecting rod**
$$\omega_{C.R} = \frac{\omega \cos \theta}{\sqrt{n^2 - \sin^2 \theta}}$$
- **Acceleration of connecting rod**
$$\alpha_{C.R} = -\omega^2 \sin \theta \left[\frac{n^2 - 1}{(n^2 - \sin^2 \theta)^{3/2}} \right]$$
- **Fluctuation of speed** $= \omega_{max} - \omega_{min}$
- **Coefficient of fluctuation of speed for fly wheel:**

$$C_s = \frac{N_{max} - N_{min}}{N} \quad N = \frac{N_{max} + N_{min}}{2}$$
- **Fluctuation of energy** $\Delta E = E_{max} - E_{min}$
- **Coefficient of fluctuation of energy for fly wheel**
$$C_E = \frac{E_{max} - E_{min}}{W_{cycle}}$$

$$\Delta E = I\omega^2 C_s$$
- **Natural frequency of spring**

$$\omega_n = \sqrt{\frac{K}{m}} \text{ rad/sec} \quad \& \quad F_n = \frac{1}{2\pi} \sqrt{\frac{K}{m}} \text{ Hz}$$
- **Damping factor**
$$\xi = \frac{C}{C_c}$$
- **Critical damping constant**
$$C_c = 2m\omega_n$$
- **Logarithm decrement**
$$= \frac{2\pi\xi}{\sqrt{1 - \xi^2}}$$
- **Transmissibility**
$$= \frac{\sqrt{1 + \left(2\xi \frac{\omega}{\omega_n} \right)^2}}{\sqrt{\left[1 - \left(\frac{\omega}{\omega_n} \right)^2 \right]^2 + \left(2\xi \frac{\omega}{\omega_n} \right)^2}}$$
- **Damped frequency**
$$\omega_d = \omega_n \sqrt{1 - \xi^2}$$